

L. 810 Injection molding  
HW #6 - Solutions

III

Problem 1.) a)  $T_{mold} = 30^\circ\text{C}$   $D = 2\text{cm}$

$T_{\text{wall}} = 100^\circ\text{C}$   $L > D$

$T_{\text{final}} = 37^\circ\text{C}$

$$\theta = \frac{T - T_{\infty}}{T_i - T_{\infty}} = \frac{(37 - 30)^\circ\text{C}}{(100 - 30)^\circ\text{C}} = \frac{1}{10}$$



For constant temp. mold  $Bi = \frac{k}{h r_0} = 0$

$\frac{r}{r_0} = \theta$  @ centerline

From Fig. 5.8 in "Transient Conduction" handout:  $F_0 \approx 0.5$  for a cylinder

$$F_0 = \frac{\alpha t}{r_0^2}$$

$$0.5 = \frac{(10^{-3} \text{ cm}^2/\text{s}) t}{(1\text{cm})^2}$$

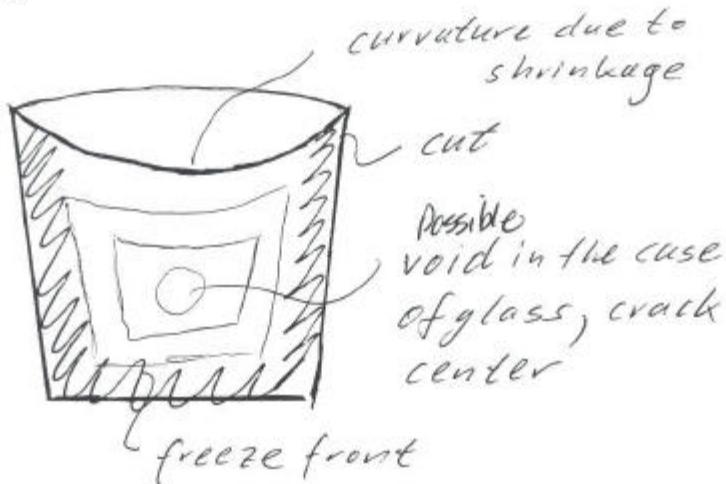
$$\Rightarrow t = 500\text{ s}$$

If  $L$  and  $D$  were of the same order then the heat loss to the mold thru the bottom surface would become significant relative to the heat loss thru the sides. Cooling time would be reduced.  
*cont'd*

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Problem #1) (cont)

b) Solidified Candle w/  $L = D$



Wax next to walls solidifies first. Wax in center cools and shrinks causing a depression. Finally case of "hydrostatic tension" may occur in very center which is last to solidify and is constrained by neighbouring already solidified material.

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Problem 2.)

## 1) Cooling Time

max. wall thickness:  $D = 0.16 \text{ cm}$ 

$$\Rightarrow D/2 = L = 0.08 \text{ cm}$$

from handout  $t_{\text{cool}} \approx \frac{L^2}{\alpha}$

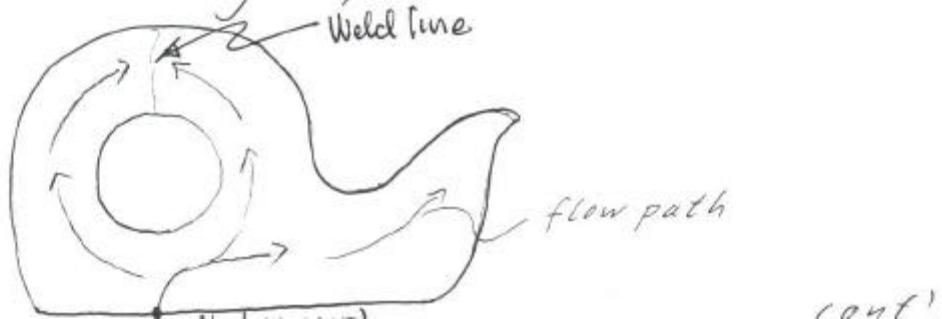
with  $\alpha \approx 10^{-3} \text{ cm}^2/\text{s}$  diffusivity for polymers

$$\Rightarrow t_{\text{cool}} = 6.4 \text{ s}$$

## 2) Special Features

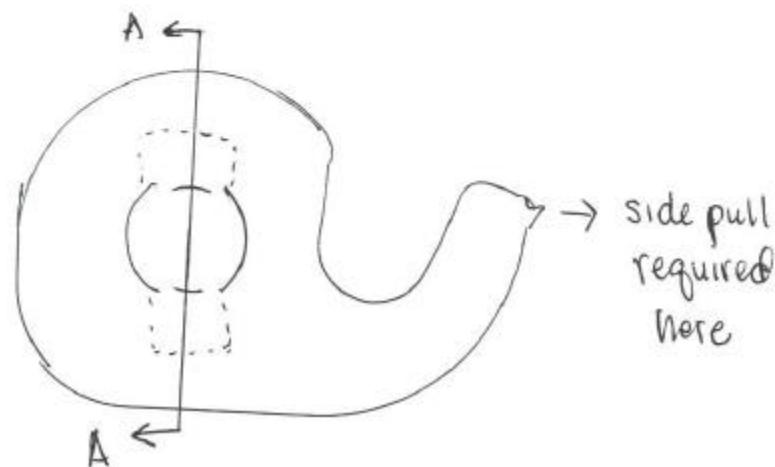
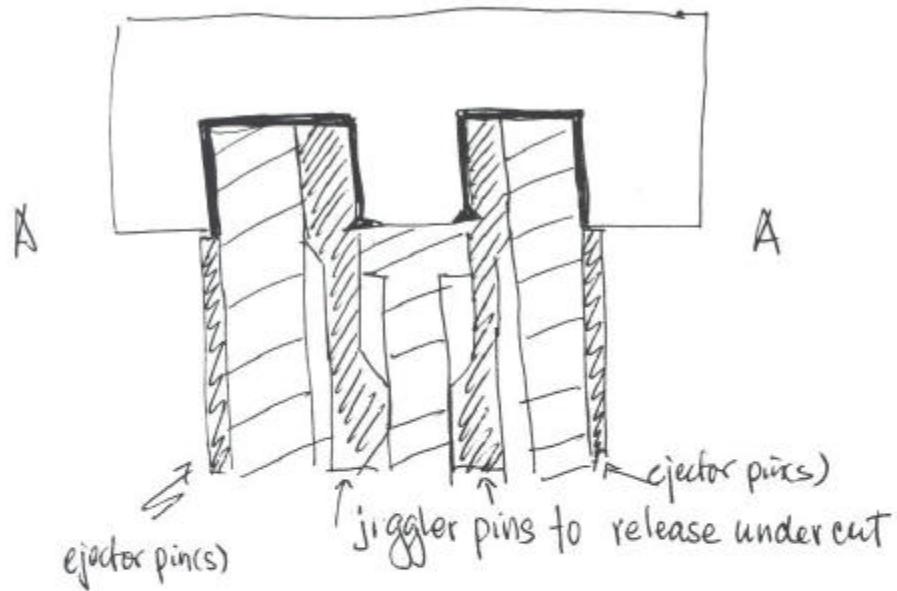
- 2 undercuts require special tool features
- serrated edge requires side pull
- ejector pins to remove part (see attached drawing)

## 3) Mold Filling Sequence



# Some features of the tooling for the plastic tape dispenser

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Problem 2) cont'

4) Machine Requirements

$$\text{Clamp Force} : F = p \cdot A_{\text{proj}} \cdot n_{\text{cavities}}$$

$$\text{injection pressure} : p \approx 10,000 \text{ psi}$$

$$\text{projected area} : A \approx 2.5 \times 2.5 \text{ in}^2 = 6.25 \text{ in}^2$$

$$\text{number of cavities} : n_{\text{cav}} = 4 \text{ (assume here)}$$

$$\Rightarrow F = 250,000 \text{ lbf} \approx 125 \text{ tons}$$

(Note: conservative estimate, large area includes runner, 10ksi probably on high side  
Shot size see Boothroyd, Dewhurst & Knight p.332 in handout)

$$\text{wt/part} = 0.502 \Rightarrow 4 \text{ cavities} = 2.008 \text{ wt}$$

$$2.008 \text{ wt} \cdot 20 \text{ oz/g} = 56 \text{ g}$$

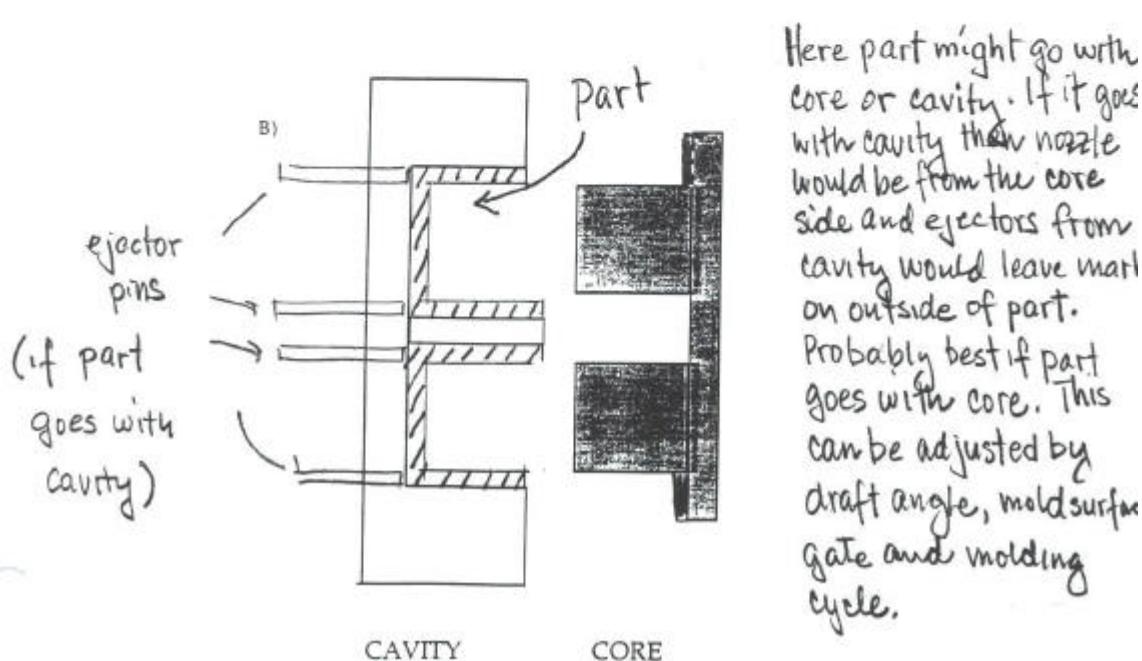
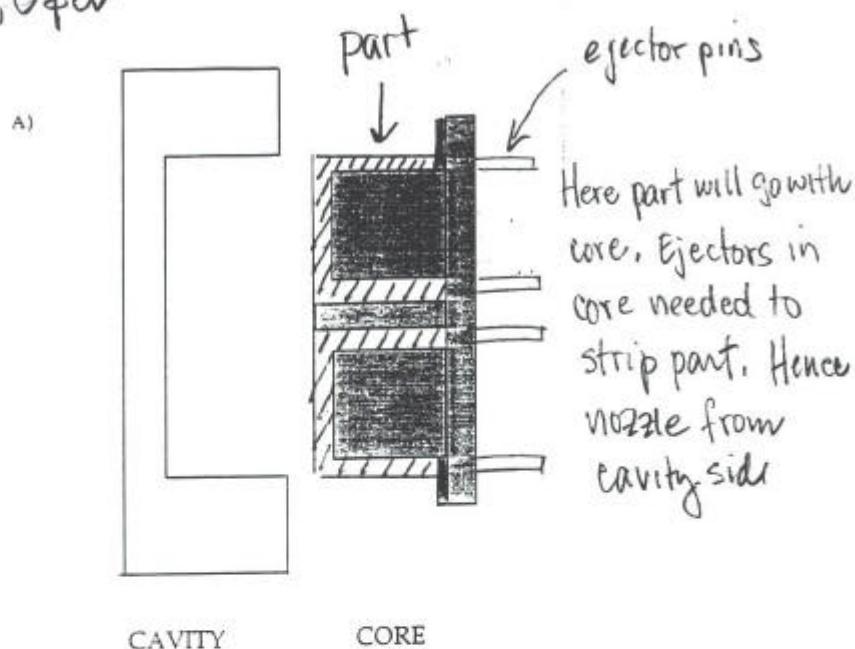
$$56 \text{ g} / 1.3 \text{ g/cm}^3 = \underline{43.1 \text{ cm}^3} \approx \underline{1.43 \text{ oz.fl}}$$

A shot size of at least 1.43 oz.fl. is required to injection mold 4 parts at once. Note: LMP Machine: 1.5 oz.

Note that runner system may add something like 37% for a 16 cm<sup>3</sup> part - our parts are 14 cm<sup>3</sup> each. See Table 8.2 in Boothroyd, Dewhurst & Knight handout.

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#3 a, c & d

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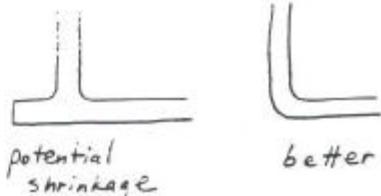


# Injection Molding Homework Solution L/W #6

Problem #3/b)

## Design Alterations / DFM

- a.) Add draft angle
- b.) Round corners
- c.) Make walls same thickness
- d.) Eliminate "overhang" if possible



## Estimate Part Cycle Time:

$$t \cong \frac{H^2}{\alpha} = \frac{(0.635 \text{ cm}/2)^2}{(10^{-3} \text{ cm}^2/\text{sec})} = 101 \text{ sec.}$$

(This time is too long, so redesign with thinner walls and ribs if necessary to stiffen.)

## Clamping Force (not asked for, but here it is)

$$\begin{aligned} \text{Projected area} &\cong (4.50 + 0.50) \times (3.50 + 0.50) \\ &\cong 20 \text{ in}^2 + \text{runner} \end{aligned}$$

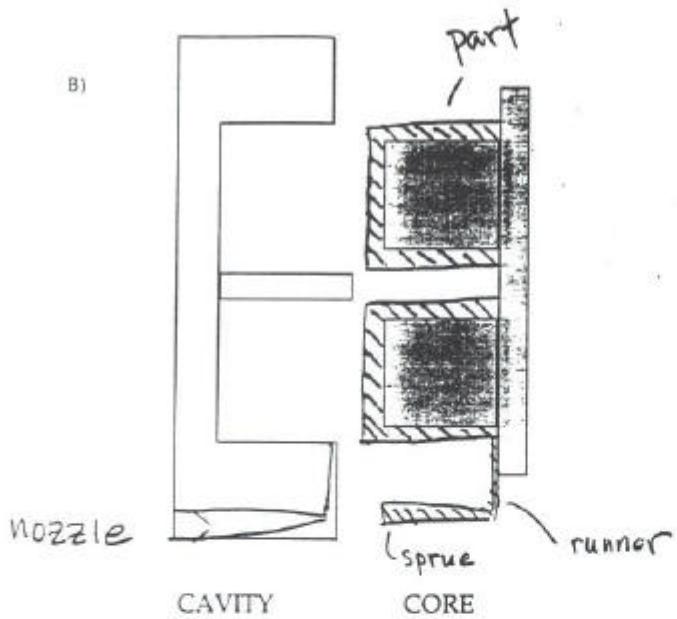
$$\text{Pressure} \cong 7000 \text{ psi}$$

eliminate in  
redesign

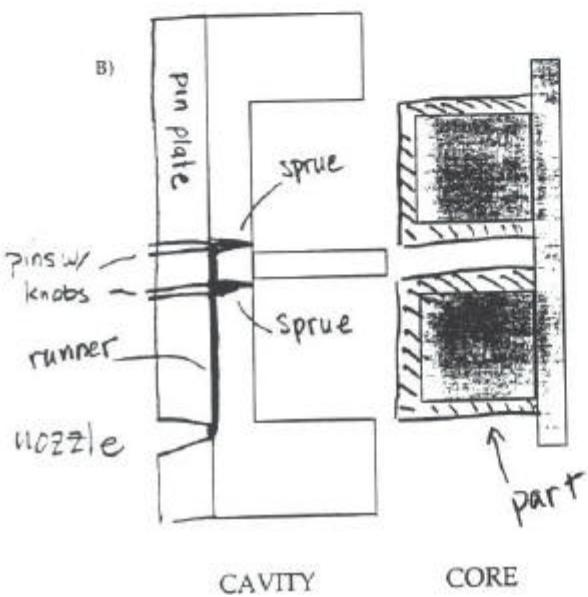
$$\begin{aligned} \text{Clamp force} &\cong 20 \text{ in}^2 \times 7000 \frac{\text{lbf}}{\text{in}^2} = 140,000 \text{ lbf} \\ &= 70 \text{ tons} \end{aligned}$$

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3e)



3f



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#4 Consider transport rate/ cooling rate (units  $\frac{1}{\text{time}}$ )

for injection molding

$$\begin{aligned} \text{transport} \quad \frac{1}{t} &\sim \frac{V}{L_x} \rightarrow \frac{1}{4} \frac{V L_z}{\alpha} \cdot \frac{L_z}{L_x} \\ \text{Cooling} \quad \frac{1}{t} &\sim \frac{\alpha}{(L_z/2)^2} \end{aligned}$$

$$\begin{aligned} \text{typical values are} \quad \frac{1}{4} & \frac{\frac{10 \text{ cm}}{s} \times 0.1 \text{ cm}}{10^{-3} \frac{\text{cm}^2}{\text{s}}} \times \frac{0.1 \text{ cm}}{10 \text{ cm}} \\ & \approx 2.5 \end{aligned}$$

Hence the two rates are about equal  
within one order of magnitude.

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for die casting typical values are,

$$\frac{1}{4} \times \frac{\frac{10 \text{ cm}}{5} \times 0.1 \text{ cm}}{0.3 \frac{\text{cm}^2}{\text{s}}} \times \frac{0.1}{10} = 10^{-2}$$

Hence the heat transfer rate is much faster and there is the danger of a thin runner system from solidifying before the molds are filled. (Note that the actual situation is a little better than this because the heat transfer rate is smaller due to film resistance)

Note that the multicavity tool for die casting shown in Fig 4 does not show overflow well commonly use. See p.413 handout Design for Die Cas

W/II

5) eqn 8.5 in Boothroyd et al is

$$t_c = \frac{h_{\max}^2}{\pi^2 \alpha} \ln \frac{4(T_i - T_m)}{\pi(T_x - T_m)}$$

let  $\frac{T_x - T_m}{T_i - T_m} = 0.1$

$$\begin{aligned} t_c &= \frac{h_{\max}^2}{4\alpha} \times \frac{4}{\pi^2} \ln \frac{40}{\pi} \\ &= 1.03 \times \frac{(h_{\max}/2)^2}{\alpha} \end{aligned}$$